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Acoustic Tweezing and Patterning of Concentration Fields in Microfluidics

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We demonstrate theoretically that acoustic forces acting on inhomogeneous fluids can be used to pattern and manipulate solute concentration fields into spatiotemporally controllable configurations stabilized against gravity. A theoretical framework describing the dynamics of concentration fields that weakly perturb the fluid density and speed of sound is presented and applied to study manipulation of concentration fields in rectangular-channel acoustic eigenmodes and in Bessel-function acoustic vortices. In the first example, methods to obtain horizontal and vertical multilayer stratification of the concentration field at the end of a flow-through channel are presented. In the second example, we demonstrate acoustic tweezing and spatiotemporal manipulation of a local high-concentration region in a lower-concentration medium, thereby extending the realm of acoustic tweezing to include concentration fields.

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I. INTRODUCTION

Sparked by the ambition to dynamically manipulate microparticles in solution, there have been major advances in the development of experimental methods to control ultrasound acoustic fields at the microscale [1,2]: for example, using bulk acoustic waves [3–5], surface acoustic waves [6–9], transducer arrays [10–12], and 3D-printed transmission holograms [13]. The acoustic radiation force acting on particles in acoustic fields is used in these systems to manipulate particles and cells, thereby concentrating [14], trapping [15,16], separating [17], and sorting [18] bioparticles and cells based on their acoustomechanical properties. It would be of considerable interest if these methods could be extended to the manipulation of solute concentration fields in microfluidic systems. Indeed, the ability to pattern and manipulate molecular concentration fields plays an essential role in several lab-on-a-chip applications and in controlled studies of biological processes such as development, inflammation, wound healing, and cancer, for which biomolecule gradients act as cellular signaling mechanisms [19]. The standard approach to precisely generate specified concentration gradients is to use microfluidic networks [20,21]—with limited temporal control, however.

Here, we present a theoretical analysis of acoustic tweezing, patterning, and manipulation of solute concentration fields in microfluidics. We predict that acoustics will offer a high degree of spatiotemporal control in these dynamical operations. Our study is predominantly motivated by the recent development of isoacoustophoresis [22], a microfluidic analog to density-gradient centrifugation. In isoacoustophoresis, cells are differentiated by their phenotype-specific acoustic impedance by observing their equilibrium position in an acoustically stabilized concentration gradient. The physics of this stabilization has only recently been understood [23], and an increased understanding of the ability of acoustics to shape and manipulate a concentration field is important to further develop the method.

In this work, we explore the consequences of our recent theory of the acoustic force density acting on inhomogeneous fluids in acoustic fields [23], a theory successfully validated by experiments, which explains the acoustic stabilization and relocation of inhomogeneous fluids observed in microchannels [24]. We define an inhomogeneous fluid as a fluid with spatial variations in density and speed of sound caused by a varying concentration of a solute. Consequently, there is a direct correspondence between fluid inhomogeneities and solute concentration. We present a theoretical framework for analyzing acoustic manipulation of such concentration fields, and we apply it to the special cases of rectangular-channel eigenmodes and Bessel-function acoustic vortices. In the former system, we present methods to obtain stable horizontal and vertical multilayer stratification of the concentration field at the end of a flow-through channel starting from typical inlet conditions. In the latter system, we demonstrate acoustic tweezing and spatiotemporal manipulation of a local high-concentration region in a lower-concentration medium. This result extends the realm of acoustic tweezing to include concentration fields.

II. MODEL SYSTEMS

In Fig. 1, the two typical model systems are introduced to provide the context necessary to appreciate the ensuing theoretical development. The implementation and design of
the numerical model and how it corresponds to experimental conditions is discussed in more detail in Sec. IV.

The first model system, shown in Fig. 1(a), is a long, straight, rectangular glass-silicon microchannel, placed along the x axis, with a piezoelectric transducer glued underneath. By actuating the transducer at a resonance frequency of the cavity, an acoustic standing-wave field can be established in the channel cross section in the y-z plane, which is typically a few hundred micrometers in the width $W$ and height $H$, leading to fundamental resonance frequencies on the order of 1–10 MHz. These systems are well characterized [4,25–28] and are used in various biomedical applications, for example, the enrichment of circulating tumor cells in blood [14,29].

The second model system, shown in Fig. 1(b), consists of a transducer array with 16 elements enclosing a circular fluid chamber. It is inspired by, and closely resembles, the experimental systems in Refs. [9,10,30–32]. The radius of these chambers is typically around 1 mm, and the chambers may have between 8 and 64 transducer elements operating at MHz frequency. By controlling the amplitude and phase of each transducer, approximate Bessel-function acoustic vortices may be generated by a superposition of waves, then used to trap and move microparticles [10,31].

III. THEORY

The recently developed theory for the acoustic force density acting on inhomogeneous fluids in acoustic fields [23] is based on the separation of time scales between the fast acoustic time scale $\tau$ and the slow hydrodynamic time scale $\tau_s$. In general, the large separation of time scales ($\tau \sim 10^3 \tau_s$) allows the acoustic fields, oscillating at the fast time scale $\tau$, to be solved for while keeping the hydrodynamic degrees of freedom fixed at each instance in time $\tau$ on the slow time scale. Because of the inhomogeneity in the fluid medium, the resulting acoustic field yields a divergence in the time-averaged acoustic momentum-flux-density tensor [23], and this is the origin of the acoustic force density $f_{ac}$, which enters the slow-time-scale hydrodynamics as an external driving force.

The inhomogeneity in the fluid medium is caused by the solute concentration field $s(r, \tau)$. The fluid density $\rho_0$, compressibility $\kappa_0$, and dynamic viscosity $\eta_0$ are all functions of the solute concentration $s$, and thus functions of space and time as the concentration field evolves by advection and diffusion,

$$\rho_0 = \rho_0[s(r, \tau)], \quad \kappa_0 = \kappa_0[s(r, \tau)], \quad \eta_0 = \eta_0[s(r, \tau)]. \quad (1)$$

The specific dependences of $\rho_0$, $\kappa_0$, and $\eta_0$ on concentration $s$ depend on the solute used to establish the inhomogeneity, e.g., iodixanol (OptiPrep), polysucrose (Ficoll), or colloidal nanoparticles (Percoll) as commonly used in density-gradient centrifugation. In this work, we consider solutions of iodixanol, for which we have measured the fluid properties as functions of concentration [22].

A. Slow-time-scale hydrodynamics

The hydrodynamics on the slow time scale $\tau_s$ is governed by the momentum and mass-continuity equations for the fluid velocity $v(r, \tau)$ and pressure $p(r, \tau)$, as well as the advection-diffusion equation for the solute concentration field $s(r, \tau)$ of the solute with diffusivity $D$,

$$\partial_\tau (\rho_0 v) = \nabla \cdot [\sigma - \rho_0 vv] + f_{ac} + \rho_0 g. \quad (2a)$$
$$\partial_\tau p_0 = -\nabla \cdot (\rho_0 v), \quad (2b)$$
$$\partial_\tau s = -\nabla \cdot [-D \nabla s + vs]. \quad (2c)$$

Here, $\mathbf{g}$ is the acceleration due to gravity, and $\sigma$ is the fluid stress tensor, given by

$$\sigma = -p \mathbf{I} + \eta_0 [\nabla v + (\nabla v)^T] + \left( \eta_0 - \frac{2}{3} \eta_0 \right) (\nabla \cdot v) \mathbf{I}, \quad (3)$$
where the superscript \( T \) indicates tensor transposition, and \( \eta_0 \) and \( \eta_0' \) are the dynamic and bulk viscosities, respectively. The equations constitute an advection-diffusion flow problem with an external forcing due to the acoustic and gravitational force densities \( f_{ac} \) and \( \rho_0 g \), both appearing on the right-hand side of the momentum equation (2a).

### B. The acoustic force density

The acoustic force density \( f_{ac} \) acting on the fluid on the slow hydrodynamic time scale \( \tau \) was derived in Ref. [23] from a divergence in the time-averaged acoustic momentum-flux-density tensor induced by continuous spatial variations in the fluid parameters of density \( \rho_0 \) and compressibility \( \kappa_0 \).

\[
f_{ac} = -\frac{1}{4} \left| p_1 \right|^2 \nabla \kappa_0 - \frac{1}{4} \left| v_1 \right|^2 \nabla \rho_0.
\] (4)

Here, \( p_1 \) and \( v_1 \) are the acoustic pressure and the acoustic velocity field, respectively, assumed to be time-harmonic first-order perturbations of the hydrodynamic degrees of freedom.

Because the compressibility \( \kappa_0 \) is difficult to measure directly, it is often more convenient to work with the fluid density \( \rho_0 \) and speed of sound \( c_0 \), both of which are readily measured as functions of concentration. With \( \kappa_0 = 1 / (\rho_0 c_0^2) \), we find

\[
\nabla \kappa_0 = \nabla \left( \frac{1}{\rho_0 c_0^2} \right) = -\kappa_0 \frac{\nabla \rho_0}{\rho_0} - 2 \kappa_0 \frac{\nabla c_0}{c_0},
\] (5)

and the expression (4) becomes

\[
f_{ac} = \frac{1}{4} \left[ \kappa_0 \left| p_1 \right|^2 - \rho_0 \left| v_1 \right|^2 \right] \nabla \rho_0 + \frac{1}{2} \kappa_0 \left| p_1 \right|^2 \nabla c_0.
\] (6)

In the weakly inhomogeneous limit where the variations in density \( \rho_0 \) and speed of sound \( c_0 \) are small, we introduce the dimensionless relative deviations \( \hat{\rho}(r, \tau) \) and \( \hat{c}(r, \tau) \) and write

\[
\rho_0(r, \tau) = \rho_0^{(0)} \left[ 1 + \hat{\rho}(r, \tau) \right], \quad \left| \hat{\rho}(r, \tau) \right| \ll 1,
\] (7a)

\[
c_0(r, \tau) = c_0^{(0)} \left[ 1 + \hat{c}(r, \tau) \right], \quad \left| \hat{c}(r, \tau) \right| \ll 1.
\] (7b)

Here, the superscript \( (0) \) indicates zeroth-order in the inhomogeneity \( \hat{\rho} \) and \( \hat{c} \). To first order in \( \hat{\rho} \) and \( \hat{c} \), the force density (6) then becomes

\[
f_{ac}^{(1)} = \frac{1}{4} \left[ \kappa_0^{(0)} \left| p_1^{(0)} \right|^2 - \rho_0^{(0)} \left| v_1^{(0)} \right|^2 \right] \nabla \hat{\rho} + \frac{1}{2} \kappa_0^{(0)} \left| p_1^{(0)} \right|^2 \nabla \hat{c}.
\] (8)

In this expression, the acoustic fields \( p_1^{(0)} \) and \( v_1^{(0)} \) are zeroth order in \( \hat{\rho} \) and \( \hat{c} \) and, consequently, the fields are obtained as solutions of the homogeneous-fluid wave equation. This constitutes a significant simplification in applications of the theory, as will be shown next.

Let \( p_a \) denote the acoustic pressure amplitude, \( \omega \) the angular acoustic frequency, and \( k_0^{(0)} = \omega / c_0 \) the homogeneous-fluid wave number. The time-harmonic acoustic fields \( p_1^{(0)} \) and \( v_1^{(0)} \) may then be written in terms of a nondimensionalized pressure field \( \hat{p}_1^{(0)}(r, \tau) \) as

\[
p_1^{(0)} = p_a \hat{p}_1^{(0)} e^{-i \omega t}, \quad v_1^{(0)} = -\frac{i p_a}{k_0^{(0)} \rho_0^{(0)}} \nabla \hat{p}_1^{(0)} e^{-i \omega t}.
\] (9)

Inserting Eq. (9) into Eq. (8) and introducing the homogeneous-fluid oscillation-time-averaged acoustic energy density \( E_{ac}^{(0)} = \frac{1}{2} k_0^{(0)} p_a^2 \), the acoustic force density \( f_{ac}^{(1)} \) can be rewritten as

\[
f_{ac}^{(1)} = E_{ac}^{(0)} \mathbf{R}(r, \tau) \nabla \hat{\rho} + C(r, \tau) \nabla \hat{c},
\] (10a)

where we have introduced the dimensionless field-shape functions \( R(r, \tau) \) and \( C(r, \tau) \), given by

\[
R(r, \tau) = |\hat{p}_1^{(0)}|^2 - (k_0^{(0)})^{-2} |\nabla \hat{p}_1^{(0)}|^2, \quad C(r, \tau) = 2 |\hat{p}_1^{(0)}|^2.
\] (10b)

The field-shape functions \( R(r, \tau) \) and \( C(r, \tau) \) depend on the shape of the homogeneous-fluid acoustic pressure field \( \hat{p}_1^{(0)}(r, \tau) \), often known analytically, and may thus be varied in space and time. Consequently, our theoretical framework suggests that a high level of spatiotemporal control of fluid inhomogeneities can be achieved.

### C. Eigenmodes in a rectangular microchannel

Consider a long, straight, hard-walled microchannel of width \( W \) and height \( H \), with the aspect ratio \( \alpha = H / W \). The acoustic fields obtained at resonance conditions in the two-dimensional channel cross section take the form of eigenmode solutions to the Helmholtz wave equation with hard-wall boundary conditions. Choosing the fluid domain in the \( y-z \) plane defined by \( 0 < y < W \) and \( 0 < z < H \), and introducing the normalized coordinates \( \hat{y} = (\pi / W) y \) and \( \hat{z} = (\pi / H) z \), the eigenmodes \( \hat{p}_1^{(0)}(\hat{y}, \hat{z}) \) are

\[
\hat{p}_1^{(0)} = \cos(n \hat{y}) \cos(m \hat{z}),
\] (11a)

with

\[
f_{nm} = \frac{\alpha_{nm}}{2\pi} = \frac{c}{2} \sqrt{\left( \frac{n}{W} \right)^2 + \left( \frac{m}{H} \right)^2}.
\] (11b)

Here, \( n = 0, 1, 2, \ldots \) and \( m = 0, 1, 2, \ldots \) are the mode numbers in the \( y \) and \( z \) directions, respectively, and \( f_{nm} \) is the resonance frequency of the \( nm \) mode.

Inserting the eigenmode solution (11) into Eq. (10), one obtains the acoustic force density acting on the fluid in the \( nm \) mode. After some algebra, the field-shape functions \( R_{nm}(\hat{y}, \hat{z}) \) and \( C_{nm}(\hat{y}, \hat{z}) \) take the form
\[ R_{nm}(\hat{r}, \hat{z}) = \frac{1}{2} \left\{ \frac{n^2}{n^2 + m^2 \alpha^2} [\cos(2n\hat{y}) - \cos(2m\hat{z})] 
+ \cos(2n\hat{y}) \cos(2m\hat{z}) + \cos(2m\hat{z}) \right\}, \quad (12a) \]
\[ C_{nm}(\hat{y}, \hat{z}) = \frac{1}{2} [1 + \cos(2n\hat{y})][1 + \cos(2m\hat{z})]. \quad (12b) \]

In the horizontal half-wave resonance \((n, m) = (1, 0)\), we obtain \(R_{10} = \cos(2\hat{y})\) and \(C_{10} = 1 + \cos(2\hat{y})\), in agreement with Ref. [23], given an appropriate change of the coordinate system.

**D. Bessel-function acoustic vortex fields**

It has been demonstrated that transducer arrays can be used to generate acoustic vortices in fluid-filled chambers [10,31–33]. By controlling the amplitude and phase of each transducer in a circular array, one can generate approximate Bessel-function pressure fields of the form [31]
\[ \hat{p}_1^{(0)} = J_1(k_0^{(0)} r) e^{i \theta}. \quad (13) \]

Here, we are using cylindrical polar coordinates \((r, \theta, z)\) with the origin at the center of the Bessel function. \(J_1\) is the 1th-order Bessel function of the first kind, and \(l\) is the number of \(2\pi\) phase shifts around the axis of the vortex, often referred to as the topological charge.

The acoustic force density acting on an inhomogeneous fluid in the acoustic vortex is obtained by inserting Eq. (13) into Eq. (10). Introducing the normalized radial coordinate \(\hat{r} = k_0^{(0)} r\) and making use of the recurrence relations \(2n/r)J_n(\hat{r}) = J_{n-1}(\hat{r}) + J_{n+1}(\hat{r})\) and \(2J_n(\hat{r}) = J_{n-1}(\hat{r}) - J_{n+1}(\hat{r})\), the field-shape functions \(R_l(\hat{r})\) and \(C_l(\hat{r})\) of the \(l\)th-order vortex take the form
\[ R_l(\hat{r}) = [J_l(\hat{r})]^2 - \frac{1}{2} [J_{l-1}(\hat{r})]^2 - \frac{1}{2} [J_{l+1}(\hat{r})]^2, \quad (14a) \]
\[ C_l(\hat{r}) = 2[J_l(\hat{r})]^2. \quad (14b) \]

**IV. NUMERICAL MODEL IN 2D**

In this section, we present the implementation and design of our numerical models. Emphasis is put on the considerations that went into designing numerical models that describe experimental conditions that may be reproduced with the setups introduced in Sec. II and sketched in Fig. 1. In order to reduce computational complexity, we model only the 2D dynamics in the perpendicular planes specified for each model in Fig. 1.

**A. Numerical implementation**

In the numerical models of the slow-time-scale hydrodynamics, the coupled field equations (2) are implemented and solved on weak form using the finite-element solver COMSOL Multiphysics [34]. We consider the limit of weakly inhomogeneous fluids and use the analytical expression (10a) for the acoustic force density \(f_a^{(1)}\) with the field-shape functions given in the rectangular-channel eigenmodes and acoustic vortex fields, respectively, in Eqs. (12) and (14).

For numerical stability, a logarithmic concentration field \(s\), with \(s = s_0 \exp(\hat{s})\), is used as the independent concentration variable. A free triangular mesh with an element mesh size around \(\Delta h = 2 \mu m\) is used. Lagrange shape functions are used with cubic-order elements in the velocity and concentration fields and quadratic-order elements in the pressure. A backward differentiation formula is used for the time stepping with an initial time step of 50 \(\mu s\) and a maximum time step of \(\Delta t = 5\) ms in all of the simulations, except that of acoustic tweezing, where the maximum time step is reduced to \(\Delta t = 0.5\) ms. These choices of parameters are motivated by the numerical stability criteria that the cell Péclet number \(Pe = U\Delta h/D\) and the Courant number \(Co = U\Delta t/\Delta h\), where \(U\) is a characteristic flow speed, should be on the order of unity or smaller.

The boundary conditions imposed on the slow-time-scale velocity and concentration fields \(v(r, \tau)\) and \(s(r, \tau)\) at the boundary \(\partial \Omega\) of the fluid domain \(\Omega\), with normal vector \(n\), are the standard no-slip and no-flux conditions,
\[ v = 0, \quad n \cdot \nabla s = 0, \quad \text{for } r \in \partial \Omega. \quad (15) \]

Several convergence tests are carried out to ensure numerical convergence. For example, the integrated concentration is conserved with a maximum relative error of \(2 \times 10^{-3}\) at all times.

**B. Modeling the fluid inhomogeneity**

We model aqueous solutions of iodixanol (OptiPrep), for which the fluid parameters have been measured experimentally as functions of the iodixanol volume-fraction concentration \(s\) [22]. OptiPrep is a cell-friendly medium that is used in density-gradient centrifugation and isoaoustic focusing. In the models, we consider initial concentration fields with iodixanol volume fractions ranging from \(s_{\text{min}} = 0.1\) to \(s_{\text{max}} = 0.3\), yielding a relative density difference of up to 10%, while the maximum relative variation in the speed of sound is 0.5%. Consequently, we neglect variations in \(c_0\), which means that only gradients in \(\rho_0\) contribute to the acoustic force density.

The polynomials fitting the measured density \(\rho_0(s)\) and dynamic viscosity \(\eta_0(s)\), as functions of the iodixanol volume-fraction concentration \(s\), are [22]
\[ \rho_0 = \rho_0^{(0)}[1 + a_1 s], \quad (16a) \]
\[ \eta_0 = \eta_0^{(0)}[1 + b_1 s + b_2 s^2 + b_3 s^3]. \] (16b)

Here, \( \rho_0^{(0)} = 1005 \text{ kg/m}^3 \) and \( \eta_0^{(0)} = 0.954 \text{ mPa s} \), and the dimensionless constants are \( a_1 = 0.522, b_1 = 2.05, b_2 = 2.54, \) and \( b_3 = 22.8 \). In Ref. [22], the diffusivity of iodixanol was measured to \( D = 0.9 \times 10^{-10} \text{ m}^2/\text{s} \). For the bulk viscosity, we use the value of pure water [35].

C. Modeling the rectangular microchannel

In this model, we consider a long, straight, rectangular microchannel of width \( W = 375 \mu \text{m} \) and height \( H = 150 \mu \text{m} \), as sketched in Fig. 1(a). In acoustophoresis experiments, acoustic eigenmodes of the two-dimensional channel cross section transverse to the flow are used extensively to manipulate and focus particles and cells based on their mechanical properties. Two notable advantages of using acoustic eigenmodes, or bulk acoustic waves, are that the eigenmodes are easily excited by an attached piezoceramic transducer actuated at the resonance frequency and that high acoustic energy densities can be obtained in the resonant modes. Typical quality factors in glass-silicon microchips are between 102 and 103, and typical measured acoustic energy densities are in the range 1–1000 J/m³ [25,27]. We use \( E_{ac}^{(0)} = 10 \text{ J/m}^3 \), approximately an order of magnitude larger than the hydrostatic pressure difference across the channel height, ensuring that gravity plays only a minor role in the fluid relocation [23].

Referring again to Fig. 1(a), we are modeling a flow-through microchannel system where the flow rate \( \Delta f \) can be controlled, thereby setting the retention time of the fluid in the channel. In our time-dependent model, the time \( \tau \) can thus be translated into a downstream length \( L \) from the inlet. For example, in the system under consideration, a fluid retention time of \( \tau_{ret} = 1.0 \text{ s} \) over a length of \( L = 5.0 \text{ mm} \) implies a flow rate of 17 \( \mu \text{l/min} \), all of which are realistic experimental parameters [22]. Diffusion generally plays a role in manipulating concentration fields. However, the time scale of diffusion across one third of the channel width is \( \tau_{diff} = (1/2D)(3W)^2 = 87 \text{ s} \), leaving enough time to conduct typical steady-flow experiments at relevant flow rates without diffusion flattening the gradients. The validity of this 2D model of the flow-through channel requires that the gradients of the concentration \( s \) in the axial direction \( \Delta s/\Delta r_\parallel \) of the flow are small in comparison to the gradients in the transverse direction \( \Delta s/\Delta r_\perp \), that is, \( |\Delta s/\Delta r_\parallel| \ll |\Delta s/\Delta r_\perp| \). Because the length scales \( \Delta r_\parallel \) and \( \Delta r_\perp \) are set by the characteristic flow speeds, the condition is that the flow speed \( U_\parallel \) in the axial direction should be much larger than the acoustically induced flow speed \( U_\perp \) in the transverse plane, \( U_\parallel \gg U_\perp \). In our simulations, considering typical experimental flow rates, \( U_\parallel \) is approximately an order of magnitude larger than \( U_\perp \).

D. Modeling the acoustic vortex field

In this model, we consider a circular fluid chamber, as sketched in Fig. 1(b), in which an acoustic vortex field of the form (13) is excited by the surrounding transducer array or by swirling surface acoustic waves [9,10,32]. Notice that, in contrast to the rectangular-microchannel acoustic fields, the acoustic vortices are nonresonant fields, and the center of the vortex can be moved relative to the chamber. In our model, we use a chamber of radius \( R = 250 \mu \text{m} \), an acoustic energy density of \( E_{ac}^{(0)} = 10 \text{ J/m}^3 \), and a frequency of \( f = 7.5 \text{ MHz} \).

V. SIMULATION RESULTS

We present a selection of simulation results demonstrating acoustics as a means to spatiotemporally control, manipulate, and relocate solute concentration fields in microsystems. Specifically, we demonstrate the manipulation of concentration fields in rectangular-concentration eigenmodes and in acoustic vortex fields in circular chambers. In the former, we demonstrate the use of sequential eigenmode actuation to obtain horizontal or vertical multilayering of the fluid inhomogeneities. We further motivate and introduce the simple but useful concept of orthogonal relocation. In the circular chamber, we demonstrate the trapping and translation of a fluid inhomogeneity using Bessel-function acoustic tweezers.

A. Multi-layering of concentration fields in rectangular-channel eigenmodes

We consider the patterning of concentration fields in the \( nm \) eigenmodes in the rectangular microchannel using the modes \((n,m) = (1,0), (2,0), (0,1), (0,2), \) and \((2,1)\) as examples. The resonance frequency \( f_{nm} \) of these eigenmodes is obtained from Eq. (11b), yielding \( f_0 = 2.0 \text{ MHz}, f_{20} = 4.0 \text{ MHz}, f_{01} = 5.0 \text{ MHz}, f_{02} = 10 \text{ MHz}, \) and \( f_{21} = 6.4 \text{ MHz} \).

In Fig. 2, we consider three different initial conditions, \( a, b, \) and \( c \) (first column), on the concentration field \( s(r,0) \). In the following columns are shown the concentration fields \( s(r,\tau) \) in the selected \( nm \) modes after a time \( \tau = 1.0 \text{ s} \) for each of the three initial configurations, \( a, b, \) and \( c \). The resulting configurations are denoted \( i = nm \), with \( i \) indicating the initial configuration \( (i = a, b, \) or \( c) \) and \( nm \) denoting the mode of actuation. The top row shows the field-shape functions \( R_{nm} \) of the corresponding modes. In general, the denser high-concentration fluid (30% iodixanol, white) is relocated into the minima of \( R_{nm} \) appearing at pressure nodes, as one might anticipate from the analogy to the acoustic radiation force acting on a particle. It should be emphasized, however, that, in contrast to the acoustic radiation force acting on a particle in a standing wave, \( f_{ac} \) is a nonconservative force and it cannot, in general, be written as the gradient of a potential. The acoustic force density \( f_{ac} \), moreover, depends on the history of the system,
which is also in contrast to the particle force. For a given mode, the concentration fields tend to evolve towards the same quasistable equilibrium configuration; however, the different initial conditions generally influence the resulting configurations.

Inspecting Fig. 2, one finds that relocation of the inhomogeneity into vertical layers is obtained for $m = 0$, while horizontal layers are obtained for $n = 0$. This result is to be expected from the geometry of the acoustic field. However, comparing $a$-01, $b$-01, and $c$-01, it is evident that the concentration field after 1 s of actuation in the 01 mode depends strongly on the initial configuration ($a$, $b$, or $c$). Indeed, configurations $a$ and $c$ have been relocated into much “cleaner” 01-mode configurations with a single horizontal layer compared to configuration $b$. The reason is that the relocations $a \rightarrow a$-01 and $c \rightarrow c$-01 are orthogonal relocations, in the sense that the initial and final stratifications are orthogonal to one another. By contrast, the relocation $b \rightarrow b$-01 is a parallel relocation, where whole fluid layers are to be moved into new parallel positions, which can only proceed by an instability. The instability is particularly evident in the 02 mode comparing the orthogonally relocated configurations $a$-02 and $c$-02 to $b$-02, the latter for which the parallel relocation proceeds by a Rayleigh–Taylor-like instability, shooting up three streams that slowly feed the second horizontal layer.

These observations suggest that orthogonal relocation provides the most effective way of relocating and patterning concentration fields. In the event that a desired relocation is parallel, as in the example $b$-01 starting from the configuration $b$, the resulting horizontally layered 01-mode configuration is blurred because it proceeds by an instability. The solution to obtaining sharp horizontally layered 01- and 02-mode configurations starting from $b$ is to go through a sequence of orthogonal relocations. By applying the sequence $b$-10-0m, the 10 mode being an intermediate, one can achieve sharp horizontally layered 0m-mode configurations from the initial configuration $b$. This operational principle is illustrated in Fig. 3, where the relocation dynamics is also indicated by showing

![Diagram](image-url)

FIG. 2. Patterning of inhomogeneous iodixanol solutions in rectangular-channel eigenmodes. The top row shows the field-shape functions $R_{nm}$ for each mode $nm$ (min, dark blue; max, light green). Three different initial concentration fields $s(r, 0)$ of the dense (30% iodixanol, white) and less dense (10% iodixanol, black) solutions are considered (first column, $a$, $b$, and $c$). The next columns show the resulting concentration fields $s(r, \tau)$ after a retention time of $\tau = 1.0$ s in either the 10 mode (second column), the 20 mode (third column), the 01 mode (fourth column), the 02 mode (fifth column), or the 21 mode (sixth column), starting from the initial condition $a$ (second row), $b$ (third row), or $c$ (bottom row).

![Diagram](image-url)

FIG. 3. Vertical and horizontal layering of iodixanol concentration fields $s(r, \tau)$ starting from the horizontally layered initial configuration $b$ with the dense fluid (30% iodixanol, white) at the bottom of the channel and the less dense fluid (10% iodixanol, black) at the top (top row). Each arrow (blue) represents an orthogonal relocation obtained by exciting an $nm$ eigenmode in the rectangular channel for 1 s, with the miniature showing the transition 50 ms after the mode shift. Vertical layering is obtained directly by actuation of the 10 or the 20 mode, yielding the configurations $b$-10 and $b$-20, respectively. Horizontal layering involves an intermediate step going through the 10 mode, yielding the $b$-10-01 and $b$-10-02 configurations.
intermediate configurations. A movie of the dynamics in the sequence b–10–01–20 can be found in the Supplemental Material [36].

In summary, starting from a single-layer configuration, one can achieve multilayering of concentration fields on a 1-s time scale in the rectangular-channel eigenmodes commonly employed in acoustophoresis. While we focus on the spatial patterning, the ability to switch between modes provides temporal control of the concentration field at the end of the flow-through channel. This type of acoustic fluid manipulation is best performed by orthogonal relocation, and a parallel relocation can always be substituted by two sequential orthogonal relocations.

B. Patterning and tweezing of concentration fields in acoustic vortex fields

Next, we demonstrate the patterning and spatiotemporal manipulation of concentration fields in Bessel-function acoustic vortex fields in circular fluid chambers. Starting from the initial concentration field \( s(r, 0) \), shown in Fig. 4(a), with the denser fluid (30% iodixanol, white) occupying half of the circular domain. Figures 4(b)–4(d) show the concentration fields \( s(r, \tau) \) after \( \tau = 3.0 \) s of actuation in acoustic vortices of orders \( l = 0 \), \( l = 1 \), and \( l = 2 \), respectively. Again, it is observed that the denser fluid tends to be relocated into the minima of the field-shape functions \( R_l \).

The central region of an acoustic vortex is of particular interest because it provides a trapping potential that can be used to trap and manipulate particles. Here, considering inhomogeneous fluid manipulation, we define the central region of the \( l \)th-order vortex from the condition \( \hat{r} < \hat{r}_l^1 \), where \( \hat{r}_l^1 \) is the first nonzero root of the field-shape function, \( R_l(\hat{r}_l^1) = 0 \). This condition yields the approximate values, \( \hat{r}_0^1 = 1.44 \), \( \hat{r}_1^1 = 1.18 \), and \( \hat{r}_2^1 = 2.26 \). As demonstrated in Fig. 4, in the vortex with \( l = 0 \), the denser fluid (white) is forced outside of the central region, while in the vortices with \( l = 1 \) and \( l = 2 \), the denser fluid is forced into the central region. Mathematically, this result follows directly from Eq. (10a) (with \( \nabla \hat{c} = 0 \)) by inspecting the field-shape functions \( R_l(r) \) shown in Fig. 4 because they indicate the initial radial distribution of the acoustic force density acting on the blurred interface. Physically, the acoustic pressure is maximum at the center for \( l = 0 \), while it is zero for \( l > 0 \). Note, furthermore, that, for \( l > 0 \), the central trapping region becomes larger for an increasing \( l \). These findings for manipulation of inhomogeneous fluids are analogous to those of the acoustic tweezing of particles [10].

Acoustic tweezing of a high-concentration region in a lower-concentration medium can thus be realized in the central region of vortices with \( l > 0 \). Hence, the central region may be used to confine and translate a fluid inhomogeneity, as will be demonstrated next using the \( l = 1 \) vortex. We consider an initial concentration field \( s(r, 0) \) that has a Gaussian-high-concentration region (30% iodixanol, white) centered at the position \( (r, \theta) = (\frac{1}{2} R, \frac{1}{2} \pi) \), as given in polar coordinates, in the lower-concentration medium (10% iodixanol); see Fig. 5(a). The width (or standard deviation) of the Gaussian is set to \( \sigma = 0.5 \hat{r}_0^1 \), half the width of the central trapping region. The acoustic vortex is initially centered at the position of the inhomogeneity, and it is then translated in a closed-loop equilateral triangle moving in straight lines from \( (\frac{1}{2} R, \frac{1}{2} \pi) \) to \( (\frac{1}{2} R, -\frac{1}{2} \pi) \) to \( (\frac{1}{2} R, -\frac{3}{2} \pi) \), and finally back to the starting position in \( (\frac{1}{2} R, \frac{3}{2} \pi) \). The translation speed \( U = 0.7 \) mm/s of the center of the vortex is chosen such that it takes 0.3 s to move the distance from one corner of the triangle to the next. The resulting concentration field \( s(r, \tau) \) after \( \tau = 0.3 \), 0.6, and 0.9 s is shown in Figs. 5(b), 5(c), and 5(d), respectively, with the central region of the vortex indicated by the green circle, and the path of the center of the vortex.
by the straight green lines. To a good approximation, the high-concentration solution is kept within the central region of the vortex as it is translated in space, leaving only a trailing diffusive residue.Movies showing the manipulation in real time for two different translation speeds are available in the Supplemental Material [36]. We find that when the translation speed of the vortex is increased by a factor of 3, the inhomogeneity does not remain trapped at the center during the full loop. Conversely, for slower translation speeds, the inhomogeneity stays in the center of the vortex, but the increased loop time leads to a more pronounced diffusion broadening.

The results presented in this section provide theoretical evidence that the applicability of acoustic tweezers can be extended beyond particle manipulation to include manipulation of concentration fields—a phenomenon that has yet to be demonstrated experimentally.

VI. DISCUSSION

In this paper, we explore some consequences of our recent theory of the acoustic force density acting on inhomogeneous fluids [23]. For this purpose, a useful formulation of the theory is given in terms of the field-shape functions $R$ and $C$ in the experimentally relevant limit of weakly inhomogeneous fluids. The theory of the acoustic force density acting on inhomogeneous fluids show resemblance to the Gorkov theory of the acoustic radiation force acting on a particle [37], for example, by the tendency of dense fluids being focused at the pressure nodes. However, the two theories have important distinctions. (1) The theory of the acoustic force density acting on inhomogeneous fluids is a field theory with $f_{ac}$ generally acting on the fluid in every point in space, in contrast to the Newtonian theory for the radiation force acting on a point particle. (2) The acoustic force density $f_{ac}$ is a nonconservative force, and, in general, it cannot be written as the gradient of a potential, as can the radiation force on a particle in a standing wave [38,39]. Instead, one may use the field-shape functions to assess the direction and magnitude of the forces acting on the fluid for a given initial concentration field. For density inhomogeneities, the denser fluid tends to relocate to the minima of the field-shape function $R$. (3) Not unrelated, in the theory of the acoustic force density, the force density $f_{ac}$ depends on the history of the system and it evolves as the concentration field changes by advection and diffusion.

While the acoustic force density can stabilize a fluid inhomogeneity against destabilizing forces, such as gravity in the case of a density gradient, it cannot counteract molecular diffusion. Consequently, an inhomogeneity always has a finite lifetime set by the characteristic diffusion time, and it will broaden due to diffusion. Interestingly, diffusion is an advantage in isoacoustic focusing because it allows fine-tuning of the gradient at the end of a steady-flow-through channel by varying the flow rate [22]. In acoustic tweezing of a high-concentration region, diffusion limits the time that the inhomogeneity can be manipulated in a closed chamber. One can obtain longer diffusion times by going to larger scales or by using Ficoll or Percoll solutions with larger solute molecules that diffuse slower.

Importantly, the ability to manipulate concentration fields requires that the concentration field introduces inhomogeneities in the fluid density or the speed of sound. A weaker inhomogeneity will, in general, result in weaker acoustic forces acting on the fluid. This scaling sets a lower limit to the weakness of an inhomogeneity that can be manipulated because, at some point, the fluid manipulation speed $U_{ac}$ becomes smaller than the speed $U_{diff}$ of the diffusing concentration profile. One may estimate the critical density deviation $\rho_{crit}$ at which manipulation becomes impossible by the condition $U_{ac} = U_{diff}$. Balancing the magnitude of the acoustic force density with the viscous shear stress, one obtains $U_{ac} \sim E_{ac} \rho' / \eta_0$, where $\rho'$ is a characteristic length scale. Equating $U_{ac}$ with the...
characteristic diffusive speed $U_{\text{diff}} \sim D/\bar{\varepsilon}$, one obtains the rough estimate $\dot{\rho}_{\text{cr}} \sim \eta_0 D / (E_{\text{ac}} \bar{\varepsilon}^2) \sim 10^{-4}$, where the number is for $\bar{\varepsilon} = 10 \, \mu$m. In practice, for the manipulation to be effective, the manipulation speed should be at least an order of magnitude larger than the diffusion speed. Consequently, for the parameters used in this study, the density deviation should be larger than 0.1% in order that the fluid can be manipulated. Note that, for concentrations of iodixanol (OptiPrep), polysucrose (Ficoll), or colloidal nanoparticles (Percoll), all used in density-gradient separation, this requirement is easily fulfilled. One can, in principle, enable manipulation of any specific solution of biomolecules at low concentration by adding a density modifier that increases the acoustic contrast to other fluids.

**VII. CONCLUSION**

Advances in the development of experimental methods to control acoustic fields for microparticle-manipulation purposes—for example, using transducer arrays, surface acoustic waves, and transmission holograms—allow spatiotemporal tailoring of acoustic fields. In this paper, we demonstrate theoretically that this tailoring provides dynamic control of solute concentration fields at the microscale. We can think of this as acoustic “landscaping” of concentration fields because of the ability to dynamically manipulate “hills” and “valleys” of high and low concentration. Using acoustic landscaping, one may relocate, shape, and pattern concentration fields with the methods already developed for particle handling as demonstrated by our two examples: First, in rectangular microchannels, we describe an operational principle for obtaining multilayer stratification of concentration fields using acoustic eigenmodes. Second, we demonstrate acoustic tweezing and manipulation of a high-concentration fluid region in a lower-concentration fluid medium using a Bessel-function acoustic vortex.

We envision that the insights obtained in this study will find applications in the further development of isoacoustophoresis and other gradient-based separation methods. Another use may be found in studies of biological processes with active spatiotemporal control of solute gradients. Finally, the ability to pattern fluid inhomogeneities using acoustics might also find applications in drug delivery, tissue engineering, and the 3D printing of microstructures.

[18] C. Grenvall, C. Magnusson, H. Lilja, and T. Laurell, Concurrent isolation of lymphocytes and granulocytes using


