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Kunov-Kruse, Andreas Jonas; Jakobsen, Peter Westergaard; Riisager, Anders; Mossin, Susanne; Fehrmann, Rasmus

Published in:
Chemistry: A European Journal

Link to article, DOI:
10.1002/chem.201601166

Publication date:
2016

Document Version
Peer reviewed version

Citation (APA):
Absorption and oxidation of nitrogen oxide in ionic liquids

Andreas J. Kunov-Kruse[a], Peter L. Thomassen[a], Anders Riisager[a], Susanne Mossin[a],*, Rasmus Fehrmann[a]

Abstract: A new strategy for capturing nitrogen oxide, NO from the gas phase is presented. Dilute NO gas is removed from the gas phase by ionic liquids at ambient conditions. The nitrate anion of the ionic liquid catalyzes the oxidation of NO to nitric acid (HNO₃) by atmospheric oxygen in the presence of water. The nitric acid is absorbed in the liquid up to approximately 1 mol HNO₃ per mol of ionic liquid due to the formation of hydrogen bonds. The nitric acid can be desorbed by heating, regenerating the ionic liquid with excellent reproducibility. Here, time resolved in-situ spectroscopic investigations of the reaction and products are presented. The procedure reveals a new vision for removing the pollutant, NO, by absorption into a non-volatile liquid and converting it into a useful bulk chemical, HNO₃.

Introduction

The man made emission of NOₓ (N₂O, NO, NO₂) is of environmental concern since NOₓ participates in detrimental photochemical reactions in both the troposphere and the stratosphere.[1] NOₓ reacts with hydrocarbon containing pollutants to form health-threatening smog in densely populated areas, as well as being active in depleting the ozone layer. The end product, NO₂, contributes to acid rain. To remove the NOₓ from flue gases, ammonia or hydrocarbons are generally used as reductants in the excellently performing SCR reaction. This technology is, however, not attractive for specialized applications, e.g. for NO removal on ships or in biomass fired and co-fired power plants, where an end-of-pipe cleaning technology is preferred.

The unique properties of ionic liquids (ILs) include high thermal stability, practically no vapor pressure and a large electrochemical window.[2–5] Recent research has focused on the use of ILs for selective absorption of acidic gasses such as CO₂ and SO₂.[6–8] In addition a recent comprehensive review on gas solubilities in ILs concerns not only CO₂ and SO₂ but reports also on all other gases known to solubilize in ILs.[9] It is remarkable that no data on NO solubilities in ILs are reported so far. SO₂ capture by ILs is suggested to depend later on the partial pressure of NOₓ with the anion of the IL.[10] This has later been confirmed by X-ray investigations of crystalline [TMGH][Cl-SO₂ (TMGH = 1,1,3,3-tetramethylguanidinium).[11] CO₂ capture by ILs similarly depends on association between the CO₂ molecules and the IL cations.[12] The bonds formed are often relatively weak and therefore, the gas can be easily expelled from the IL in a regeneration step. Water is inevitably present in a flue gas and since water also interacts with the anion of the IL,[13] water is a likely inhibitor in both cases. Oxygen from the flue gas may also interfere with the absorption.[13] Here a different strategy to remove NO and NO₂ from a gas stream is proposed, where the water and oxygen present are actively utilized to chemically convert the NOₓ into nitric acid, HNO₃, which then accumulates in the IL due to the formation of strong hydrogen bonds.[14]

The current work present in-situ Attenuated Total Reflectance Fourier Transform Infrared (ATR-FTIR) spectroscopic results of interaction between a thin IL film and a combined gas stream containing dilute NO gas, atmospheric air and water. From time-resolved experiments mechanistic evidence for the oxidation and absorption reactions as well as the stoichiometry of the absorption have been extracted. The accumulated HNO₃ can be desorbed by heating the IL above 120 °C. The IL is completely regenerated with no trace of decomposition products observed.

Results and Discussion

A thin film of IL was monitored with ATR-FTIR spectroscopy during exposure to a controlled gas flow containing NO. A schematic of the setup is shown in Fig. S1 (Supporting Information). The influence of cations and anions of the IL on the reactivity was also investigated. The employed cations are depicted in Chart 1.

The characteristic IR bands observed and monitored during the reactions were: Nitrate (NO₃⁻): 1340 cm⁻¹ (vs); nitric acid (HNO₃): 948 cm⁻¹ (s), 1660 cm⁻¹ (s); water (H₂O): 3400 cm⁻¹ (s), 1640 cm⁻¹ (s); dinitrogen tetroxide (N₂O₄): 1858 cm⁻¹ (w), 1750 cm⁻¹ (vs), 948 cm⁻¹ (s), 1660 cm⁻¹ (s); acetate (CH₃COO–): 1550 cm⁻¹ (vs) and acetic acid (CH₃COOH): 1710 cm⁻¹ (vs).[15,16] The bands corresponding to nitrate (NO₃⁻) were: 750 cm⁻¹ (w); nitrate (NO₃⁻) was also investigated. The employed cations are depicted in Chart 1.
the reaction proceeds without O\textsubscript{2}. No reaction was observed when \[\text{BMIM}\][\text{NO}_3] was first left to equilibrate with the atmosphere and then exposed to NO (10 % v/v) for 80 minutes (Fig. S2). Therefore the disproportionation of NO and the presence of a NO\textsubscript{2} impurity in the gas stream are both dismissed as the reason for the observed activity. A control experiment with dry NO and O\textsubscript{2} on a dry IL film was also performed and we could determine that the reaction was indeed slower when water was the limiting factor. The only source for the protons in the observed HNO\textsubscript{3} was water present either in the IL or in the gas phase and no other type of reactivity was observed in experiments with NO gas. If NO, O\textsubscript{2} and H\textsubscript{2}O are all present the characteristic HNO\textsubscript{3} bands appear within minutes of exposure of the IL film to 1. Thus it was concluded that HNO\textsubscript{3} is only formed when all three components are present simultaneously.

**In-situ ATR-FTIR experiments**

A thin film of [BMIM][NO\textsubscript{3}] was applied to the diamond surface of the IR cell and exposed to a gas stream containing different concentrations of NO (1-6 % v/v) in combination with O\textsubscript{2} (8-18 % v/v), water (~1 % v/v) and balance N\textsubscript{2} at different temperatures. When applied, the IL forms a thin film on the diamond minimizing mass transfer limitations. Thus, the experiment is envisioned as a model for the interaction between the gas phase and a supported ionic liquid phase (SILP) material. The IR spectra obtained for the 2 % v/v NO experiments at room temperature (RT) are shown in Fig. 1. The characteristic very intense band at ~1340 cm\textsuperscript{-1} of the nitric acid immediately decreases in intensity as acidic protons become available (see Chart 2). Additionally, the nitrate band splits as less symmetric hydrogen bonded species are generated, giving bands at 1426, 1330, 1295 and 1250 cm\textsuperscript{-1}, see Fig. 1. Similarly, within 20 sec of gas exposure the characteristic peaks of the solvated HNO\textsubscript{3} molecule at 940 and 1660 cm\textsuperscript{-1} increase in intensity. An isosbestic point is clearly observed at 1400 cm\textsuperscript{-1}. Another isosbestic point at 1300 cm\textsuperscript{-1} is less well defined due to weak intensity peaks from HONO at 1260 and 1290 cm\textsuperscript{-1}. The presence of isosbestic points confirm that essentially only two forms of the nitrate ion exist in the solution; free as in pure [BMIM][NO\textsubscript{3}] and in a strong hydrogen bond with HNO\textsubscript{3}. A reference experiment was performed in order to assess whether the reaction proceeds without O\textsubscript{2}. No reaction was observed when [BMIM][NO\textsubscript{3}] was first left to equilibrate with the atmosphere and then exposed to NO (10 % v/v) for 80 minutes (Fig. S2). Therefore the disproportionation of NO and the presence of a NO\textsubscript{2} impurity in the gas stream are both dismissed as the reason for the observed activity. A control experiment with dry NO and O\textsubscript{2} on a dry IL film was also performed and we could determine that the reaction was indeed slower when water was the limiting factor. The only source for the protons in the observed HNO\textsubscript{3} was water present either in the IL or in the gas phase and no other type of reactivity was observed in experiments with NO gas. If NO, O\textsubscript{2} and H\textsubscript{2}O are all present the characteristic HNO\textsubscript{3} bands appear within minutes of exposure of the IL film to 1. Thus it was concluded that HNO\textsubscript{3} is only formed when all three components are present simultaneously.

**[BMIM][CH\textsubscript{3}COO]**

The experiment using [BMIM][CH\textsubscript{3}COO] is shown in Fig. 2. Initially, a prominent water band at 3400 cm\textsuperscript{-1} (not shown) was present since [BMIM][CH\textsubscript{3}COO] is hygroscopic and has a significant content of water when in equilibrium with the atmosphere. It was eroded quickly as the reaction progressed. The prominent acetate bands at 1570 and 1380 cm\textsuperscript{-1} disappeared within a few minutes, while a band from acetic acid concurrently appeared at 1710 cm\textsuperscript{-1}. After longer time of exposure, the HNO\textsubscript{3} bands appeared and bands corresponding to both acids coexisted. After gas exposure for more than 5 minutes (or after gentle heating to 80 °C) the acetic acid was lost, as indicated by the disappearance of the bands assignable to both acetate and acetic acid. Hence, only the bands from nitric acid and hydrogen bonded nitrate remained. When heated to 120 °C the nitric acid bands were finally also completely lost, and the resulting spectrum features again the characteristic nitrate band at 1340 cm\textsuperscript{-1} corresponding to the spectrum of pure [BMIM][NO\textsubscript{3}]. The minor differences were assigned to the different water content of the ILs. Desorption is gradual and most of the nitric acid is desorbed before 120 °C. Interestingly, the temperature of complete desorption corresponds to the boiling temperature of the azeotrope of nitric acid and water (bp 121 °C), whereas pure nitric acid boils at 83 °C. On the other hand, water and acetic acid (bp 118 °C) do not form an azeotrope and the complete loss of acetic acid was accordingly observed at significantly lower temperatures.
**ATR-FTIR spectrum of [BMIM][CH₃COO] exposed to a gas stream containing NO (6 % v/v), O₂ (8 % v/v) and water (∼1 % v/v) at RT.** The dotted line corresponds to the spectrum of pure IL exposed to air saturated with water, whereas the grey and black solid lines correspond to the spectra recorded after 7 and 12 min gas exposure, respectively. The dash-dot line corresponds to the spectrum recorded after heating to 120 °C and subsequent cooling to RT.

**A similar experiment for [BMIM]Cl is shown in Fig. 3.** Here the bands from the cation are more readily identified. The final spectrum obtained after exposure to NO, O₂ and H₂O was identical to the spectrum recorded in the [BMIM][NO₃] experiments. The absence of isosbestic points, however, indicates the formation of an intermediate. The strong band at 1360 cm⁻¹ identifies the intermediate as a non-hydrogen-bonding nitrate anion (*vide infra*).

**ATR-FTIR spectrum of [EMIM][CF₃SO₃] exposed to a gas stream containing NO (6 % v/v), O₂ (8 % v/v) and water (∼1 % v/v) at RT.** The dotted line corresponds to the spectrum of pure IL, the solid black line to the spectrum of the saturated IL at steady state (17 min) while the grey lines correspond to intermediate spectra. The dash-dot line corresponds to the spectrum after heating to 120 °C and subsequent cooling to RT.

**[BMMIM][NO₃]**

The C2 position of the IL imidazolium ring can be deprotonated when the anion of the IL is a strong base, and the formed carbene have been shown to be reactive towards CO₂.[21] In order to discard an analogous reaction path in the current study, IR experiments were also performed with [BMMIM][NO₃] having a methyl group in the C2 position of the imidazolium ring. The obtained spectral results (Fig. S3, Supporting Information) were identical to the results for [BMIM][NO₃], validating that the carbene reaction path is not relevant. Hence, all experimental results suggested that the [BMIM]⁺ cation does not partake in the reaction. The non-involvement of the cation was further confirmed in experiments performed with acetate and nitrate based ILs containing the cheap, biodegradable and non-toxic cholinium cation (Chart 1). The results are shown in Figures S4 and S5 (Supporting Information) and are analogous to the ones for imidazolium ILs with the same anion.
[BMIM][NO₃] and NO₂

Using dry NO₂ gas instead of NO the experiment with [BMIM][NO₃] was repeated (Fig. 5). NO₂ was willingly absorbed in the IL and dimerized in the condensed phase, giving characteristic peaks from N₂O₄ at 1858(w), 1750(vs) and 750 (w) cm⁻¹.[22] Bands from HONO and HNO₃ were also prominent after absorption, indicating disproportionation of N₂O₄ in the presence of water in the IL. When the gas feed was changed to dinitrogen saturated with water, the bands specific for N₂O₄ decreased immediately and the characteristic HNO₃ bands increased.

Quantification of HNO₃

A standard curve for determination of the HNO₃ concentration in the IL was generated by measuring IR spectra of solutions prepared by dissolving known amounts of concentrated nitric acid in [BMIM][NO₃] at RT (Fig. S6, Supporting information). Either of the HNO₃ bands at 1660 and 948 cm⁻¹ can be used to quantify the amount of HNO₃ present in the IL, but since a water band overlaps with the former band the results obtained using the latter were more reliable and reproducible. Importantly, all conclusions are equally valid from quantification of the 1660 cm⁻¹ band. The IR spectrum in the vicinity of the characteristic HNO₃ vibrations at 948 cm⁻¹ were deconvoluted by Gaussian functions, using the method described previously.[23] The area under the Gaussian function fitted to the 948 cm⁻¹ band in the experimental spectrum can be correlated to the HNO₃ content by use of the standard curve. The uncertainty of the total HNO₃ content determined by this method is estimated to be 10-20 % based on the quality of the reference spectra and the fitting procedure.

The fitting procedure was applied to all time-resolved spectra at RT of [BMIM][NO₃], [EMIM][CF₃SO₃], [BMIM]Cl, [Ch][CH₃COO] as well as [BMMIM][NO₃] when exposed to NO (6 % v/v) with O₂ and water in excess. The results are shown in Fig. 6. For the cholinium based ILs, IR bands from the cation are overlapping with the quantifiable HNO₃ bands. By careful use of the peak deconvolution method reliable data were obtained. The steady state saturation point approximately corresponds to a molar ratio of 1.1:1 (HNO₃:IL) for the acetate, chloride and nitrate ILs, respectively, whereas the triflate IL converges at a ratio of approximately 0.6. The apparent difference in absorption rate observed between [BMIM][NO₃] and [BMMIM][NO₃] was due to a difference in the absorption setup and is not considered to be significant. The time resolved spectra of [BMIM][NO₃] were measured with an improved setup allowing the IL to be exposed to the NO/O₂/H₂O mixture exactly at t = 0, whereas the switch for the other ILs was dependent on replacement of a non-negligible volume of gas before the ATR cell resulting in a concentration gradient during the first minutes of the experiment. Accordingly, the time line has been shifted 20 sec to partially correct for this. All experiments performed under identical conditions support the conclusion that the cation does not influence the rate of absorption or the obtained molar ratio of HNO₃ to IL.

The IL anion, on the other hand, is decisive for the evolution of the spectra. The acetate IL shows conversion of NO to HNO₃ as fast as the nitrate IL, whereas the triflate IL shows a slower conversion. The slow rate of accumulation of HNO₃ in [BMIM][CF₃SO₃] is assigned to triflate being less nucleophilic towards activation of NO. Evaluation of the IR spectra of the IL suggests that HNO₃ forms hydrogen bonds to other HNO₃ molecules, weak hydrogen bonds to the oxygen atoms in the triflate anion, and none to the fluorine atoms which are very poor hydrogen bond acceptors. Triflate is the anion of a stronger acid than HNO₃, and is not protonated during the reaction.

Notably, the chloride IL has a significantly different overall profile with an initial induction period followed by a slow conversion to HNO₃ before reaching a molar HNO₃/IL ratio of about 1.2 for H₂O to Cl⁻. This is much higher than for any of the other ILs used (~1 % w/w H₂O for [BMIM][NO₃]).

Figure 6: Integrated area of the 948 cm⁻¹ HNO₃ band as function of exposure time to a gas stream containing NO (6 % v/v), O₂ (8 % v/v) and water (~1 % v/v) at RT. The area is converted to mole ratios using the standard curve given in Fig. S6 (Supporting Information). The experiment with [BMIM][NO₃] was...
performed with the gas above the IL changing immediately to the target composition. All the other experiments were performed with a more gradual change of the gas flow.

After the first minutes of gas exposure some water was likely driven out of the liquid and the reaction also consumed water resulting in the 3400 cm\(^{-1}\) water band decreasing fast. All protons generated in the reaction became bound to chloride leaving no protons to generate HNO\(_3\). Accordingly, a relatively narrow band corresponding to non-hydrogen bonded nitrate appears in Fig. 3 in the time interval corresponding to 50–150 sec in Fig. 6 and the apparent rate of generation of HNO\(_3\) is lower. After 150 sec the rate of HNO\(_3\) formation in [BMIM]Cl increases sharply to the same value as for [BMIM][CH\(_3\)COO], [BMIM][NO\(_3\)], [Ch][NO\(_3\)] and [BMIM][NO\(_3\)] and the band of the non-hydrogen bonded nitrate disappears.

The rate of accumulation of nitric acid in the IL is very dependent on the NO concentration as well as the temperature. [BMIM][NO\(_3\)] was saturated with HNO\(_3\) at room temperature after 50 sec when exposed to 6 % v/v NO, excess O\(_2\) and water. With 1 % v/v NO it took 3000 sec. In the in-situ ATR-IR experiments the maximal linear rate of increase in intensity of the HNO\(_3\) band was determined. The experiment was performed multiple times with different NO concentrations at RT and the measured rates are plotted in Fig. 7, top. From these experiments an apparent order of the reaction with respect to NO was determined to be 2.0 (±0.3).

Once the IL is saturated with HNO\(_3\) the reaction cannot be followed further with IR performed on the IL film, but the reaction between NO and HNO\(_3\) is likely to continue although at a significantly lower rate. The IL provides a sticky surface where NO from the gas phase can react with HNO\(_3\) giving NO\(_2\) and HNO\(_2\), which are liberated to the gas stream if the IL is locally saturated. However, the liberated species might be absorbed further downstream.

The absorption of NO by the ILs is very temperature dependent giving rise to a decrease in the absorption capacities with increasing temperature (Fig. 7, bottom). The solubility of gasses in ILs generally decrease with increasing temperature.\(^{[26]}\) We expect the same to be the case for NO, NO\(_2\) and O\(_2\). On the other hand, the rate of NO oxidation is expected to increase with temperature. Due to the two competing effects it was not possible to generate an Arrhenius plot for the total reaction based on the experiments described here. The overall maximum rate was observed around 30 °C. We assume that the rate of the NO oxidation reaction is limiting the overall rate below this temperature, and that the solubility of the reactants in the IL determines the overall rate above this temperature.

**Bulk experiments**

Absorption followed gravimetric

Absorption of NO in [BMIM][CH\(_3\)COO] and [BMIM][NO\(_3\)] was performed by passing the gas slowly through bulk ILs (~1 g) in two types of experiments. The gas uptake was followed gravimetrically. Series 1 was performed with 10 % v/v NO in N\(_2\) bubbling through [BMIM][CH\(_3\)COO] at 100 °C for about 10 days to obtain steady state. The resulting solution was allowed to cool to RT under continuous gas exposure. Time 0 was chosen as the point when the solution was at RT. The solution was left with time to equilibrate. After several days a new steady state had been reached (Fig. 8). Oxygen and water was not deliberately added in this experiment, since it was originally intended as a pure NO absorption experiment. Series 2 is a reproduction of series 1 with a different batch of IL. In series 3, pre-dried [BMIM][NO\(_3\)] was bubbled through with a gas stream of 5 % v/v NO containing water and oxygen in excess (1 % v/v and 10 % v/v, respectively). The weight was followed closely until steady state. Despite the difference in conditions for series 1 and 2 compared to series 3 an identical weight increase compared to time t = 0 was found at steady state.
The observations are explained in the following way: In the initial stages of series 1 and 2 some water is present in the [BMIM][CH$_3$COO] and the precautions to keep out oxygen and water over an extended period were not sufficient. Thus NO is being oxidized to HNO$_3$, which is a stronger acid than acetic acid and [BMIM][CH$_3$COO] + HNO$_3$ will give [BMIM][NO$_3$] + CH$_3$COOH. The generated acetic acid is not retained in the liquid at 100 °C and is lost to the gas phase with time. At steady state the conversion is complete. This is in correspondence with the observation of the viscosity of the IL changing drastically since [BMIM][NO$_3$] has a much lower viscosity than [BMIM][CH$_3$COO] due to a weaker hydrogen bonding pattern between cation and anion. After the temperature is lowered to RT the starting point in series 1, 2, and 3 are now analogous. Series 3 reaches steady state faster since the access to oxygen and water is not limited by diffusion through tubing or presence as impurity in the gasses or setup. The end point after waiting to steady state is the same for series 1, 2 and 3. Thus we conclude that the reactivity observed for series 1 and 2 is the same as for series 3 despite the initial difference in IL and reaction conditions.

Comparison between IL and aqueous nitrate solution

It is relevant to compare the reaction rates of uptake and oxidation of NO in IL media to the one in an analogous aqueous nitrate solution in order to prove that the IL is in fact enhancing the reaction rate and not just providing a non-volatile reaction medium. Unfortunately it is not possible to design a comparable experiment using neither the in-situ FTIR setup nor the gravimetric analysis of absorption in bulk sample. The water in the aqueous nitrate solution will evaporate fast leaving just the nitrate salt on the IR diamond and, in the bulk experiment, evaporation of water will change the weight of the solution. Instead the reactions were compared by quantifying the developed acidic protons by volumetric analysis as follows. In series 4, a solution of NaNO$_3$ in water having the same molar concentration of nitrate as [BMIM][NO$_3$] (approx. 6 M) was prepared. NO (5 % v/v) and air saturated with water was bubbled through 3.0 mL of the solution at 10 mL/min in a series of experiments. After 2, 4, 6, 8 and 10 hours, respectively, the gas flow was stopped and the solution was diluted with degassed water. Thymol blue was added as acid/base indicator and titration was performed with a 0.10 M NaOH solution. In series 5 the same experiments were performed on [BMIM][NO$_3$]. Both series 4 and 5 showed an increasing amount of acidic protons being accumulated in the liquids, as a function of the exposure time. The higher viscosity of the IL should result in hindered mass transfer across the gas/liquid interface compared to an aqueous NaNO$_3$ solution. Despite this effect favoring the conversion in the aqueous solution it was observed that the IL had accumulated approximately 3 times as many acidic protons as the aqueous nitrate solution during the first couple of hours (see Figure S10, Supporting Information). After longer experiments, the IL approaches saturation and reacts slower whereas the aqueous solution continues to have a linear increase. Water evaporating from the aqueous solution during the experiment was partially avoided using a low flow rate and the air in the flow being saturated with water. Nevertheless some water loss could not be avoided judged by the weight change of the solution. The aqueous solution produces some precipitate of NaNO$_3$ with time since the solubility is exceeded locally. This is not a problem for the IL where no precipitates are observed. The

TGA

Thermogravimetric analysis (TGA) performed on the pure [BMIM][CH$_3$COO] compared to the product after steady state confirms the transformation of the IL (see Fig. S7, Supporting Information). [BMIM][NO$_3$] decomposes at temperatures well above 240 °C, which is 60 °C higher than the decomposition temperature of [BMIM][CH$_3$COO].

NMR

$^1$H and $^{13}$C NMR analyses (in CDCl$_3$ and DMSO-d$_6$) were performed on the bulk [BMIM][CH$_3$COO] sample after absorption to steady state with NO at room temperature and subsequent desorption for 3 h at 100-110 °C (without gas flow). The data were compared to the NMR spectra of pure [BMIM][NO$_3$] (Figs. S8 and S9, Supporting Information) and were found to be almost identical. The spectra revealed no indication of proton or carbon signals attributed to acetic acid (these would be found at $\delta$(H)/ppm = 2.1 (3H), 11.4 (1H); $\delta$(C)/ppm = 20.8 (CH$_3$), 178.1 (COOH)) in the sample after desorption. On the other hand, some well-defined signals at $\delta$(H)/ppm (CDCl$_3$) = 13.8 and $\delta$(H)/ppm (DMSO-d$_6$) = 5-6 (broad) were observed indicating that desorption of HNO$_3$ was not complete. No decomposition products were observed in the NMR spectra after this absorption-desorption cycle, and the chemical shifts of the imidazolium cation signals remained essentially unchanged compared to the pure [BMIM][NO$_3$], except for a slight upfield shift (0.05-0.20 ppm) of the aromatic protons caused by the acidic environment.

Figure 8: Increase in mass of bulk ILs as a function of time by passing a gas through the IL via a sintered glass fit at RT. The gain of mass is assumed to be due to HNO$_3$ only and has been recalculated to a mole fraction of HNO$_3$ relative to the IL. In series 1 and 2 [BMIM][CH$_3$COO] was exposed to a gas flow of 10% v/v NO in N$_2$ at 100 °C for several days before cooling to RT (at t = 0) under continued gas flow. In series 3, pre-dried [BMIM][NO$_3$] was exposed to a gas mixture of 5% v/v NO with excess O$_2$ and water at RT.
use of a frit section at the end of the gas tube inserted in the aqueous solution provided irreproducible results as sodium nitrate precipitates in the frit. Therefore an open-end (Ø1 mm) glass tube was used for both experiments.

Comparison between inert gas, NO, CO₂ and SO₂
In a realistic flue gas CO₂ and SO₂ are also present and can interact with the ionic liquid. In order to separately assess the interactions of these gasses with the ionic liquid the following control experiments were performed: 5 different gas mixtures was bubbled through ~1 g of initially dry [BMIM][NO₃] at 40 mL/min. See Table 1 and Figure S11.

<table>
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<th>Experiment no.</th>
<th>1</th>
<th>2</th>
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In the first three experiments the weight increase is only water since acid-base titration reveals that the amount of acidic protons in the solutions after absorption is close to 0. For experiment 4 with 5 % NO the IL is almost saturated after 6 h and the increase in both weight and acidity of the solution is very high. For experiment 5 with 1000 ppm NO the results show that the reaction does take place but the saturation is slow due to the low concentration of NO. The weight increase is not significantly higher than for 1-3 but acidic protons corresponding to 10 % of the molar amount of IL was found after 36 h. This corresponds to ~15 % of the NO in the total gas volume that was bubbled through 1 g of IL for 36 h.

Discussion
The cations of the ILs do not decompose even when heated to 120 °C in concentrated nitric acid, the original IR spectra of the nitrate and triflate ILs are completely recovered after cooling to RT even after many cycles. If bulk [BMIM][NO₃] saturated with HNO₃ is kept completely dry and heated to above 120 °C for longer periods some yellow coloration is observed, but no irreversible decomposition products have been observed. When exposing [BMIM]Cl to NO, species corresponding to both hydrochloric acid and nitric acid are present in the solution, but the IL does not decompose despite being saturated with this very potent oxidation mixture. These observations show that the ILs have excellent chemical stability towards H₃N₂O₂ species. This is rationalized with the imidazolium ring being well protected from electrophilic attack by NO₂⁺ or similar species due to its positive charge. As seen from the proposed reaction pathway below, radicals originating from dioxygen are not believed to be part of the turnover of the reaction. The fact that the organic cations are unaffected by the harsh treatment is also a strong indication that the formation of uncontrollable reactive radical species is controlled in the IL media by the more stable radicals NO and NO₂. Unprotected organic molecules or other impurities present in the IL are likely less protected and therefore oxidized and decomposed completely to CO₂ and water giving a self-cleaning process of the IL during heating to the regeneration temperature.

NO₂ is always present to some extent in pressurized NO gas bottles due to the slow, but irreversible disproportion reaction of NO to form N₂O and NO₂.[26] However, since no HNO₃ formation was observed in absence of dioxygen in the feed gas (Fig. S2, Supporting Information), the disproportion reaction cannot account for the observed generation of HNO₂. Similarly, the level of autoxidation of NO by dioxygen in the gas phase before contact with the IL was monitored with gas-phase UV-Vis and found to be very low and thus not responsible for the observed reactivity. Furthermore, preliminary[27] and ongoing investigations of the gas conversion reaction with supported ionic liquid phase (SILP) absorbers reveal a much higher conversion dynamics over the IL phase compared to bypass experiments. So far several absorption (at RT) – desorption (at 130 °C) cycles performed by SILP absorbers revealed completely reversible and unchanged capacity of the absorber.

Proposed reaction cycle
The overall reaction (1) is thermodynamically favored with ∆G = -210 kJ mol⁻¹, but it is very slow at ambient conditions.

4 NO(g) + 3 O₂(g) + 2 H₂O(l) → 4 HNO₃(l) (1)

ILs have ion strengths which are of course much higher than for molecular liquids and higher than brine solutions as well. For ILs consisting of large organic cations and small inorganic anions, the base strength and the nucleophilicity of the anion is much higher than if the anion was solvated in water.[26] Normally, NO is kinetically inert toward many common reactants but ILs provide a condensed medium containing strong nucleophiles. The absence of a full hydration shell decreases the activation barrier for nucleophilic attack. Based on the experimental evidence given here a mechanism for the oxidation reaction of NO in IL is suggested.

The oxidation of NO is reported in the literature to have the same rate law (2) in gas phase and in aqueous solution despite the total reactions being different.[28,29] In this work a second order dependence on ρ(NO) over the IL film was also found (see Fig. 7), and we expect the same rate law is relevant for the rate-determining step in this IL solution.

\[ \frac{d[NO]}{dt} = k[NO]^2[O_2] \] (2)

Gas phase:
2 NO(g) + O₂(g) → 2 NO₂(g) (3)

Aqueous solution:
4 NO(g) + O₂(g) + 2 H₂O(l) → 4 H⁺(aq) + 4 NO₂⁻(aq) (4)

In ILs an adduct can form between the IL anion and the NO molecule capturing and activating the NO for further reactions,
since the anion is a powerful base and nucleophile. In the case of a nitrate IL the attack on NO can involve oxidation of the NO nitrogen which is thermodynamically favored. The product has one negative charge and is likely to be caught in the IL phase and to participate in further reactions. The initiation step in the condensed IL phase is thus proposed to be:

\[
\text{NO(g)} + \text{NO}_3^-(\text{IL}) \rightarrow \text{N}_2\text{O}_5^-(\text{IL}) \tag{5}
\]

The unstable adduct \(\text{N}_2\text{O}_5^-(\text{IL})\) is then suggested to decompose to two species with the intermediate oxidation states of +III and +IV (6). Reactions (5) and (6) are analogous to the reaction between NO and HNO\(_3\) in the atmosphere or on surfaces.\(^{[30–33]}\), (6). Reactions (5) and (6) are analogous to the reaction between two species with the intermediate oxidation states of +III and +IV (6).

\[
\text{N}_2\text{O}_4^-(\text{IL}) \rightarrow \text{NO}_2^-(\text{IL}) + \text{NO}_2^+(\text{IL}) \tag{6}
\]

It was shown (see Fig. 5) that NO\(_2\) dimerizes to N\(_2\)O\(_4\) in the IL when insufficient water is present (7).

\[
2 \text{NO}_2^-(\text{IL}) \rightarrow \text{N}_2\text{O}_4^-(\text{IL}) \tag{7}
\]

We expect N\(_2\)O\(_4^-\) to be able to disproportionate to ions in an ionic media (8). This corresponds to the anhydrous form of the known disproportionation reaction occurring on surfaces.\(^{[34]}\)

\[
\text{N}_2\text{O}_4^-(\text{IL}) \rightarrow \text{NO}_2^-(\text{IL}) + \text{NO}_2^+(\text{IL}) \tag{8}
\]

Two nitrite anions from (6) or (8) could hypothetically be oxidized by O\(_2\) in one step (9):

\[
2 \text{NO}_2^-\text{(IL)} + \text{O}_2(g) \rightarrow 2 \text{NO}_3^-\text{(IL)} \tag{9}
\]

However, reaction (9) is probably not very favored even in an IL phase since two anionic species have to be close together in order to allow reaction with one O\(_2\) molecule. Under dry conditions, the final products after complete oxidation are the ionic species NO\(_2^-\) and NO\(_3^-\), as in the solid state of N\(_2\)O\(_5\).

In the majority of the experiments enough water was present allowing reactions (10)-(12) to take place and several of the intermediates are observed in Fig. 5.

\[
\begin{align*}
\text{N}_2\text{O}_4^-(\text{IL}) + \text{H}_2\text{O(IL)} &\rightarrow \text{HNO}_2^-(\text{IL}) + \text{HNO}_3^-(\text{IL}) \tag{10} \\
\text{HNO}_2^-(\text{IL}) &\rightarrow \text{NO}_2^-\text{(IL)} + \text{H}^+(\text{IL}) \tag{11} \\
\text{HNO}_2^-(\text{IL}) + \text{NO}_3^-\text{(IL)} &\rightarrow \text{H}_2\text{O} + \text{HNO}_3^-\text{(IL)} \tag{12}
\end{align*}
\]

The protons generated will prefer NO\(_2^-\) over NO\(_3^-\) since nitrite is the stronger base. The dimeric species HN\(_2\)O\(_4^-\) (IL) and the nitrous acid dimer have a strong hydrogen bond keeping the two nitrogen(III) species close together. The nitrog(III) species have thus been activated for oxidation by dioxygen in one step. The product is the analogous nitric acid-nitrate dimer:

\[
\text{HN}_2\text{O}_4^-(\text{IL}) + \text{O}_2(\text{IL}) \rightarrow \text{H}_2\text{O} + \text{HNO}_3^-\text{(IL)} \tag{13}
\]

This corresponds well to the observed ∼1:1 molar ratio between HNO\(_2^-(\text{IL})\) and HNO\(_3^-(\text{IL})\) after gas saturation. When the IL is saturated with HNO\(_3\), there are just enough protons to allow every proton to form a strong hydrogen bond between two nitrite anions. No free basic nitrite anions are then available for nucleophilic attack on NO\(_2^-\), only allowing HNO\(_3^-\) to accumulate very slowly in the IL after this point (see Fig. 7). The nitrate-nitric acid dimer is clearly observable in the IR spectrum and is the final product until the nitric acid is desorbed by raising the temperature:

\[
\text{HN}_2\text{O}_5^-(\text{IL}) \rightarrow \text{HNO}_3^-\text{(IL)} + \text{NO}_3^-\text{(IL)} \tag{14}
\]

An analogue to reaction (13) has previously been suggested to explain why the rate of oxidation of NO\(_3^-\) by dioxygen was observed to be several orders of magnitude faster just around 0 °C in water droplets.\(^{[35,36]}\) The freeze-concentration effect leads the HNO\(_2^-(\text{IL})\) concentration to increase drastically in the remaining liquid phase by a factor of 240-11000.\(^{[15]}\) The formed HNO\(_2^-\) dimers are activated towards oxidation by O\(_2^2^-\):

\[
\text{(HONO)}_2^-(\text{aq}) + \text{O}_2(\text{aq}) \rightarrow 2 \text{HNO}_2^-\text{(aq)} \tag{15}
\]

In the IL phase a single proton assures that nitrogen(III) species are held together, activating them towards oxidation by O\(_2\) in an analogous manner.

Reaction (13) is suggested to be the rate-determining step after a series of pre-equilibria: (5)-(7) and (10)-(12). This is in accordance with the overall reaction order of two with respect to NO. The complete reaction pathway consisting of reactions (5)-(7) and (10)-(14) is shown in the catalytic cycle in Scheme 3, having the stoichiometry of the total reaction in reaction (1). The individual reactions with coefficients are listed in Table S1 (Supporting Information). The appearance of the cycle is complicated by the demands of stoichiometry and the suggestion of elementary reactions but can be considered in a simple way as nitrate oxidizing NO to HNO\(_3\) and thereby being reduced itself to nitrite. O\(_2\) then reoxidizes nitrite to nitrate regenerating the catalyst.

![Scheme 3: Stoichiometric reaction cycle for the oxidation of NO to HNO\(_3\) catalyzed at RT by nitrate based ILs (reactants and products are in bold).](image-url)
corresponding nitrate IL after one cycle. Acetate is a very powerful Lewis and Brønsted base in a pure IL[24] and FTIR measurements performed on [BMIM][CH₃COO] (Fig. 2) and [Ch][CH₂COO] (Fig. S4, Supporting Information) show that IR features assignable to acetate at 1550 cm⁻¹ decrease very quickly as nitrate and acetic acid bands increases. As NO is absorbed and oxidized, nitric acid is formed but the protons are already immediately removed by acetate. Judged from the decreasing intensity of the band at 1715 cm⁻¹ with time, the acetic acid is slowly removed from the liquid even at RT. In the bulk experiments with [BMIM][CH₃COO], acetic acid was absent according to NMR analysis after one absorption-desorption cycle. When starting from a more basic anion than nitrate, it is suggested that the generated, unprotonated nitrate anion is involved in the further absorption and oxidation of NO. Furthermore, as acids accumulate in the IL, the nitric acid will be retained more strongly than the other acids due to its formation of a high-boiling azeotrope with water having a pattern of strong hydrogen bonds.

Conclusions

Nitrate is a catalyst for the oxidation of NO by O₂ to nitric acid. Nitrate is reduced to nitrite by NO and is reoxidized by O₂ restoring the catalyst. Aqueous nitrate solutions have modest activity towards this reaction. By using a nitrate based ionic liquid, the catalyst is an integral part of the reaction medium, the reaction is at least three times faster than in aqueous solution with comparable nitrate concentration, and, most importantly, the reaction can be run in a continuous flow without the reaction media being lost by evaporation. Under exactly the same conditions the IL does not absorb either CO₂ or SO₂ to any measurable extent. Interconversion between the different nitrogen species in the condensed IL phase is likely dynamic and fast and the concentrations are the equilibrium values. The most reactive species towards oxidation by dioxygen is expected to be a nitrite-nitrous acid adduct or a nitrous acid dimer. Both are formed by two electrons to a dioxygen molecule and make the corresponding dimeric nitrogen(V) species without oxygen radical intermediates. The hydrogen bonds formed serve to retain the nitrogen species in the IL phase removing them from the gas phase. This method is therefore a tool to absorb exhaust NO₂ species from off gasses and storing them. The absorption ability can be restored in a desorption step at higher temperatures. No deterioration of the absorption properties of the IL is observed even after many absorption-desorption cycles. After saturation all nitrate ions participate in strong hydrogen bonds and the molar ratio between NO₃⁻ and HNO₂ is ∼1:1. Thus, the resulting mixture after saturation with HNO₂ can be formulated as a new IL: [BMIM][NO₃]·HNO₂. The product after desorption is a concentrated HNO₃ stream that can be condensed with water as nitric acid of commercial grade. The cation of the IL has no apparent influence on the absorption reaction and in most cases the anion is converted to nitrate after one absorption-desorption cycle. Thus, ILs like the non-toxic cholinium chloride used as a vitamin additive for livestock is expected to be just as effective as traditional imidazolium-based IL and can be obtained at a much lower cost.

In order to overcome the mass-transfer limitations for the interaction of bulk ILs with the gas phase, solid absorbers with ILs impregnated on porous silica or other porous supports can be made. The resulting SILP materials[25,27] are very promising for the application as reversible NO₂ absorbers in end-of-pipe installations of industrial units emitting NOₓ like, e.g. power plants, ships and cement factories. Investigations with such SILP absorbers are ongoing.

Experimental Section

[BMIM][NO₃] (>98%, IoLiTec), [BMIM][CH₃COO] (>98%, Sigma-Aldrich), [BMIM][Cl] (95%, Sigma-Aldrich), [BMIMIM][NO₃] (>98%, IoLiTec), [Ch][CH₂COO] (95%, Sigma-Aldrich) and [EMIM][CF₃SO₃] (>99%, IoLiTec) were obtained from commercial sources and used as received. [Ch][NO₃] was produced in-situ by exposing [Ch][CH₂COO] to a gas mixture of NO/O₂/water in nitrogen followed by heating to 120 °C in a flow of nitrogen.

The gas streams were mixed from 10 % v/v NO in N₂, N₂, CO₂, 2 % v/v SO₂ in N₂ and air. All gases were delivered by AGA. The gas flow was controlled by mass flow controllers (Bronkhorst). To obtain a wet gas the air or N₂ stream was led through water or D₂O (99.9%, Sigma-Aldrich) in a bubble flask fitted with a glass frit and joined with the NO gas just before the reactor. NO and O₂ was led through stainless steel tubing (Swagelok) close to the reactor chamber in order to minimize autoxidation of NO in the gas phase which is facilitated by sunlight. NO₂ was generated by heating copper metal with HNO₃ (65 %, Sigma-Aldrich). Prior to subjecting the IL sample to the gas, the gas was dried through a column with activated molecular sieves (4 Å). ATR-FTIR experiments were performed on a Nicolet iS5 spectrometer equipped with a thermoregulated (up to 300 °C) Specac Golden Gate High Temperature diamond ATR cell. This was fitted with an add-on cap, allowing the controlled gas mixture to flow over the diamond of the instrument at atmospheric pressure (Fig. S7, Supporting Information). The experiments were performed with 1-8.5 % v/v NO, 8-20 % v/v O₂, 1-1.5 % v/v water at 50 mL/min. The IL was applied as a thin film in the center of the diamond before securing the add-on cap. For IL screening experiments, the gas exchange was performed with a valve outside the add-on cap and a reproducible delay before the reaction was present. The time resolved experiments with [BMIM][NO₃] were performed with the atmosphere in the cap being equilibrated before quickly adding the cap over the IL film on the ATR diamond. The reaction and absorption was followed in real time by recording spectra continuously. For each spectrum, 4-16 scans with 4 cm⁻¹ resolution (approximately 5-20 s measuring time) were performed. The spectra were background and ATR corrected in OMNIC 8.2 assuming a refractive index of 1.5 and a reflectance angle of 90°. Gaussian deconvolution using PeakFit[20] was performed individually in the area of the 948 and 1660 cm⁻¹ peaks of HNO₃. To allow for batch deconvolution, a method was developed for Gruplot 4.1.[26] Further details on the deconvolution method can be found in literature.[21] The shown full spectra in Figure 1-6 were all obtained at RT. Spectra (not shown) obtained at temperatures up to 60 °C were the basis for the results shown in Figure 7, bottom.

The bulk experiments were performed in 5 series in a 15 mL custom made cylindrical Schlenk flask fitted with a tube (with or without a glass frit) reaching almost to the bottom and valves both on the inlet and outlet.
Enough liquid is added to cover the opening of the insert so the gas is passing through the liquid. After closing the valves, the entire flask can be disconnected from the gas line and weighed.

For series 1 and 2, [BMIM][CH$_3$COO] (1 mL) were used. For series 3 and 5, [BMIM][NO$_3$] (1 mL and 0.9 mL, respectively) were used. For series 4, NaNO$_3$ (2 mL, 6M) in degassed water were used. The gasses were pure 10 % v/v NO at 10 mL/min for series 1 and 2; 5 % v/v NO, 10 % v/v O$_2$ and -1 % v/v water at 30 mL/min for series 3; and 5 % v/v NO, 10 % v/v O$_2$ and -1 % v/v water at 10 mL/min for series 4 and 5. All five series were followed gravimetrically by weighing several times. In series 1 and 2 the reaction vial was submerged in an oil bath at 100 °C while under the gas flow for several days to obtain steady state. Then the oil bath was removed and the flask cooled down to RT. Still under flow, a new steady state was obtained at room temperature after several days. Series 3 were performed at RT and followed by weighing multiple times. Series 4 and 5 consists of several individual experiments at RT which were stopped after 2, 4, 6, 8 and 10 hours, respectively, by adding a total of 50 mL degassed water in several portions and transferring the resulting solution to an Erlenmeyer flask. Thymol blue was added as acid/base indicator and the amount of acidic protons were determined by titration with NaOH (0.100 M). For series 4 and 5 the experiments were reproduced with an open end glass tube. This had little influence for the experiments with IL but problem with clogging of the frit with NaNO$_3$ in the aqueous solution bulk experiments were avoided giving more reproducible results.

NMR spectra were recorded at RT on a Bruker 300 MHz NMR instrument of CD$_3$Cl$_2$ solutions/inhomogeneous mixtures of pure [BMIM][NO$_3$] and [BMIM][CH$_3$COO] as well as of the ILs after saturation with NO gas in the bulk at RT as described above under sections 3 and subsequent desorption without flow at 110 °C for 3 h. [BMIM][NO$_3$] δ H/ppm (CD$_3$Cl$_2$): 0.86 (3H, butyl), 1.28 (2H, butyl), 1.78 (2H, butyl), 3.93 (3H, methyl), 4.16 (2H, butyl), 7.42 (1H, C5), 7.48 (1H, C4) and 9.62 (1H, C2); δ 13C/ppm (CD$_3$Cl$_2$): 13.5, 19.6, 32.2, 36.5, 50.1, 122.5, 123.9, 137.7 (impurities: 54.7, 104.6 ppm). [BMIM][CH$_3$COO] after reaction δ H/ppm (CD$_3$Cl$_2$): 0.92 (3H, butyl), 1.33 (2H, butyl), 1.84 (2H, butyl), 3.96 (3H, methyl), 4.20 (2H, butyl), 7.37 (1H, C5), 7.41 (1H, C4) and 9.42 (1H, C2), 13.62 (0.5 H, HNO$_3$); δ 13C/ppm (CD$_3$Cl$_2$): 13.5, 19.6, 32.2, 36.5, 50.1, 122.5, 123.9, 137.5 (impurity: 54.7).

TGA were performed on a Mettler Toledo TGA/DSC 1 STARe system in a flow of nitrogen of 70 mL/min. Samples were heated from RT to 600 °C at 10 °C/min.

Determination of water contents in the ILs were performed by Karl Fischer titration on a Metrohm 888 Titrando by analyzing 3 samples of 0.1 mL.

**Acknowledgements**

This work is financially supported by Energinet.dk through the PSO project 10521 and Copenhagen Cleantech Cluster (GAP project no. 91050-Ko). S.M thanks the Danish Independent Research Council DFF (project no. 09-070250). FP7 COST Action CM1306 EXIL is acknowledged for financial support for dissemination. Dr. Johannes Due Hansen, Thorey Grettarsdottir and Aníta Godiksen, Centre for Catalysis and Sustainable Chemistry, DTU Chemistry, Technical University of Denmark are acknowledged for performing preliminary investigations. LAB S.A. France and DONG Energy, Denmark are also thanked for financial support and valuable discussions.

**Keywords:** Ionic liquids • NO$_x$ • in situ ATR-FTIR • gas absorption • nitric acid


The answer is NO! A new vision for removing NO from exhaust gases is presented. Nitrate-based ionic liquids catalyze the fast oxidation of NO by O₂ to nitric acid, which is accumulated in the non-volatile ionic liquid to 1:1 at room temperature. The reaction is followed in-situ in a thin film by ATR-FTIR. A mechanism for the catalytic reaction is suggested revealing the importance of the anion for the reactivity of the ionic liquid.

Author(s), Corresponding Author(s)*

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